

|                 |  |
|-----------------|--|
| $\bar{V}_e$     | decrease in volume due to electrostriction |
| $V_f^o$         | limiting effective flow volume             |
| $\bar{V}_{int}$ | intrinsic volume of the amino acid         |
| $V_s$           | shrinkage volume                           |
| $V_v$           | volume associated with void                |
| $V_{vW}$        | van der Waals volume                       |
| $V_{sh}$        | volume of solvation sheath                 |

#### Greek Letters

|                       |   |
|-----------------------|---|
| $\phi_v$              | apparent molar volume   |
| $\phi_v^o$            | limiting apparent molar volume or infinite-dilution partial molar volume  |
| $\phi_v^o(\text{tr})$ | change in partial molar volume when amino acid is transferred from water to aqueous $\text{NH}_4\text{Cl}$ solution |
| $\eta$                | viscosity of solution   |
| $\eta_0$              | viscosity of pure solvent   |
| $\eta_r$              | relative viscosity ( $\eta/\eta_0$ )  |
| $\rho$                | density of solution   |
| $\rho_0$              | density of pure solvent   |

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**Supplementary Material Available:** Tables of detailed density and viscosity data for different amino acids as a function of concentration in aqueous ammonium chloride solutions (15 pages). Ordering information is given on any current masthead page.

## Viscosity and Density of Ternary Mixtures of Toluene, Bromobenzene, 1-Hexanol, and 1-Octanol

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Mixture viscosities and densities of the ternary mixtures of toluene, bromobenzene, 1-hexanol, and 1-octanol were measured at 30, 40, 50, and 60 °C. The nonidealities reflected in mixture viscosities are expressed and discussed in terms of excess viscosities, which were negative in most of the cases. The ternary  $\eta$ - $X$ - $T$  data were fitted in a Redlich-Kister-type equation along with a ternary contribution term.

#### Introduction

Extending our earlier work ( $1-\beta$ ) on viscosities and dielectric constants of liquid mixtures, the present paper reports the

viscosities and the densities for the ternary mixtures of toluene, bromobenzene, 1-hexanol, and 1-octanol in the temperature range from 30 to 60 °C.

#### Experimental Section

**Materials.** Toluene (BDH), 1-hexanol (BDH), and 1-octanol (Ferah Berlin) were fractionally distilled and dried while bromobenzene (E. Merck) after repeated fractional distillation was collected at  $156 \pm 0.5$  °C and retained for use. The mean values of repeat density, viscosity, and refractive index measurements of the liquids so purified did not deviate from the corresponding literature values beyond allowable limits (Table IV). Redistilled deionised and degassed water (electrical conductivity  $< 7.0 \times 10^{-7} \Omega^{-1} \text{cm}^{-1}$ ) was used in each case for checking the instruments and calibrating the pycnometers.

**Experimental Measurements.** Ternary mixtures were prepared by weight with an accuracy of 0.0001 g, taking care that the resulting ternary compositions represent the data points suitably distributed away from the vertices and also located in

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**Table I. Experimental Densities  $\rho_m$  and Viscosities  $\eta_m$  for the Ternary Mixture Toluene (1)-Bromobenzene (2)-1-Octanol (3) at Different Temperatures**

| no. | $X_1$  | $X_2$  | $t, ^\circ\text{C}$ | $\rho_m, \text{g mL}^{-1}$ | $\eta_m, \text{cP}$ |
|-----|--------|--------|---------------------|----------------------------|---------------------|
| 1   | 0.9033 | 0.0580 | 30                  | 0.894 81                   | 0.5587              |
|     |        |        | 40                  | 0.888 85                   | 0.5034              |
|     |        |        | 50                  | 0.882 85                   | 0.4584              |
|     |        |        | 60                  | 0.878 13                   | 0.4255              |
| 2   | 0.0561 | 0.9058 | 30                  | 1.421 7                    | 0.9434              |
|     |        |        | 40                  | 1.414 3                    | 0.8550              |
|     |        |        | 50                  | 1.411 1                    | 0.7844              |
|     |        |        | 60                  | 1.409 2                    | 0.7109              |
| 3   | 0.0782 | 0.0796 | 30                  | 0.862 59                   | 4.293               |
|     |        |        | 40                  | 0.858 12                   | 3.201               |
|     |        |        | 50                  | 0.855 45                   | 2.485               |
|     |        |        | 60                  | 0.853 49                   | 1.970               |
| 4   | 0.7518 | 0.1488 | 30                  | 0.940 19                   | 0.7752              |
|     |        |        | 40                  | 0.935 83                   | 0.6775              |
|     |        |        | 50                  | 0.932 58                   | 0.6087              |
|     |        |        | 60                  | 0.929 14                   | 0.5585              |
| 5   | 0.1446 | 0.7552 | 30                  | 1.311 7                    | 1.055               |
|     |        |        | 40                  | 1.304 6                    | 0.9341              |
|     |        |        | 50                  | 1.301 0                    | 0.8397              |
|     |        |        | 60                  | 1.299 1                    | 0.7585              |
| 6   | 0.1814 | 0.1847 | 30                  | 0.922 21                   | 2.541               |
|     |        |        | 40                  | 0.916 70                   | 2.024               |
|     |        |        | 50                  | 0.914 29                   | 1.637               |
|     |        |        | 60                  | 0.911 85                   | 1.355               |
| 7   | 0.3707 | 0.3774 | 30                  | 1.058 7                    | 1.111               |
|     |        |        | 40                  | 1.052 2                    | 0.9722              |
|     |        |        | 50                  | 1.048 2                    | 0.8615              |
|     |        |        | 60                  | 1.044 8                    | 0.7766              |
| 8   | 0.5960 | 0.2423 | 30                  | 0.992 43                   | 0.8902              |
|     |        |        | 40                  | 0.985 94                   | 0.7820              |
|     |        |        | 50                  | 0.981 65                   | 0.6958              |
|     |        |        | 60                  | 0.978 47                   | 0.6252              |
| 9   | 0.4567 | 0.4650 | 30                  | 1.136 4                    | 0.7753              |
|     |        |        | 40                  | 1.129 4                    | 0.6802              |
|     |        |        | 50                  | 1.123 5                    | 0.6360              |
|     |        |        | 60                  | 1.118 7                    | 0.6051              |
| 10  | 0.2364 | 0.6029 | 30                  | 1.201 7                    | 1.022               |
|     |        |        | 40                  | 1.194 0                    | 0.8939              |
|     |        |        | 50                  | 1.190 4                    | 0.8023              |
|     |        |        | 60                  | 1.188 0                    | 0.7275              |
| 11  | 0.1294 | 0.5222 | 30                  | 1.123 7                    | 1.495               |
|     |        |        | 40                  | 1.117 3                    | 1.253               |
|     |        |        | 50                  | 1.113 3                    | 1.084               |
|     |        |        | 60                  | 1.111 4                    | 0.9470              |
| 12  | 0.2687 | 0.2737 | 30                  | 0.978 63                   | 1.700               |
|     |        |        | 40                  | 0.971 94                   | 1.408               |
|     |        |        | 50                  | 0.967 99                   | 1.192               |
|     |        |        | 60                  | 0.965 44                   | 1.008               |
| 13  | 0.5164 | 0.1326 | 30                  | 0.913 79                   | 1.245               |
|     |        |        | 40                  | 0.908 44                   | 1.045               |
|     |        |        | 50                  | 0.905 97                   | 0.8901              |
|     |        |        | 60                  | 0.903 51                   | 0.7809              |

**Table II. Experimental Densities  $\rho_m$  and Viscosities  $\eta_m$  for the Ternary Mixture Toluene (1)-1-Hexanol (2)-1-Octanol (3) at Different Temperatures**

| no. | $X_1$  | $X_2$  | $t, ^\circ\text{C}$ | $\rho_m, \text{g mL}^{-1}$ | $\eta_m, \text{cP}$ |
|-----|--------|--------|---------------------|----------------------------|---------------------|
| 1   | 0.9479 | 0.0290 | 30                  | 0.858 69                   | 0.5190              |
|     |        |        | 40                  | 0.852 63                   | 0.4586              |
|     |        |        | 50                  | 0.847 32                   | 0.4209              |
|     |        |        | 60                  | 0.842 04                   | 0.3911              |
| 2   | 0.0389 | 0.9347 | 30                  | 0.818 05                   | 3.587               |
|     |        |        | 40                  | 0.813 45                   | 2.655               |
|     |        |        | 50                  | 0.811 27                   | 2.167               |
|     |        |        | 60                  | 0.809 74                   | 1.757               |
| 3   | 0.0479 | 0.0411 | 30                  | 0.823 97                   | 5.337               |
|     |        |        | 40                  | 0.819 51                   | 3.927               |
|     |        |        | 50                  | 0.816 80                   | 3.026               |
|     |        |        | 60                  | 0.815 22                   | 2.367               |
| 4   | 0.0825 | 0.6372 | 30                  | 0.820 79                   | 3.646               |
|     |        |        | 40                  | 0.816 37                   | 2.833               |
|     |        |        | 50                  | 0.813 55                   | 2.270               |
|     |        |        | 60                  | 0.811 21                   | 1.776               |
| 5   | 0.4176 | 0.0717 | 30                  | 0.834 64                   | 1.894               |
|     |        |        | 40                  | 0.829 86                   | 1.541               |
|     |        |        | 50                  | 0.826 55                   | 1.281               |
|     |        |        | 60                  | 0.823 62                   | 1.081               |
| 6   | 0.6442 | 0.3071 | 30                  | 0.842 86                   | 0.8856              |
|     |        |        | 40                  | 0.837 09                   | 0.7670              |
|     |        |        | 50                  | 0.832 07                   | 0.6770              |
|     |        |        | 60                  | 0.828 13                   | 0.5943              |
| 7   | 0.3941 | 0.3382 | 30                  | 0.831 47                   | 1.841               |
|     |        |        | 40                  | 0.825 19                   | 1.519               |
|     |        |        | 50                  | 0.822 13                   | 1.312               |
|     |        |        | 60                  | 0.820 01                   | 1.141               |
| 8   | 0.1655 | 0.4972 | 30                  | 0.823 77                   | 3.171               |
|     |        |        | 40                  | 0.818 37                   | 2.435               |
|     |        |        | 50                  | 0.815 03                   | 1.924               |
|     |        |        | 60                  | 0.812 90                   | 1.578               |
| 9   | 0.2384 | 0.5456 | 30                  | 0.826 26                   | 2.507               |
|     |        |        | 40                  | 0.821 67                   | 1.937               |
|     |        |        | 50                  | 0.818 67                   | 1.543               |
|     |        |        | 60                  | 0.815 26                   | 1.285               |
| 10  | 0.3331 | 0.2144 | 30                  | 0.831 23                   | 2.181               |
|     |        |        | 40                  | 0.826 55                   | 1.715               |
|     |        |        | 50                  | 0.823 56                   | 1.422               |
|     |        |        | 60                  | 0.821 38                   | 1.178               |
| 11  | 0.4811 | 0.1376 | 30                  | 0.836 69                   | 1.555               |
|     |        |        | 40                  | 0.831 34                   | 1.315               |
|     |        |        | 50                  | 0.828 85                   | 1.116               |
|     |        |        | 60                  | 0.826 19                   | 0.9454              |
| 12  | 0.5182 | 0.3812 | 30                  | 0.837 52                   | 1.211               |
|     |        |        | 40                  | 0.831 79                   | 1.008               |
|     |        |        | 50                  | 0.827 63                   | 0.8550              |
|     |        |        | 60                  | 0.824 41                   | 0.7372              |
| 13  | 0.5939 | 0.2548 | 30                  | 0.840 18                   | 1.054               |
|     |        |        | 40                  | 0.833 14                   | 0.8946              |
|     |        |        | 50                  | 0.827 94                   | 0.7658              |
|     |        |        | 60                  | 0.824 78                   | 0.6768              |

extreme corners near the vertices of the triangular composition diagram.

Ostwald viscometers were used with necessary precautions for viscometric measurements (9). The standard deviations in the time of flow was found not to exceed 0.1%. For density measurements (9), the pycnometers used were calibrated with water with 0.997 07 g mL<sup>-1</sup> as its density at 25 °C.

For temperature control, a Toshniwal Model GL-15 precision thermostat, with the bath temperature monitored to 0.01 °C with a standardized Beckmann thermometer, was used. During experiments, the bath temperature did not fluctuate beyond  $\pm 0.1$  °C and also the evaporation of experimental liquids was checked to a minimum and remained insignificant.

The viscosities and densities were considered significant to four figures.

## Results and Discussions

The viscosity and density data for the ternary mixtures toluene (1)-bromobenzene (2)-1-octanol (3), toluene (1)-1-hexanol (2)-1-octanol (3), and bromobenzene (1)-1-hexanol (2)-1-octanol (3) at 30, 40, 50, and 60 °C are presented in Tables I-III. The component mole fractions were chosen in such a way that the experimental region so identified was expected to provide convenient and meaningful data leading to suitable correlations and useful conclusions.

The experimental measurements of viscosities and densities were made at 30, 40, 50, and 60 °C. The increment in temperature level was kept regular at 10 °C to ensure measurable effects of temperature change on experimental observations.

**Table III. Experimental Densities  $\rho_m$  and Viscosities  $\eta_m$  for the Ternary Mixture Bromobenzene (1)-1-Hexanol (2)-1-Octanol (3) at Different Temperatures**

| no. | $X_1$  | $X_2$  | $t, ^\circ\text{C}$ | $\rho_m, \text{g mL}^{-1}$ | $\eta_m, \text{cP}$ |
|-----|--------|--------|---------------------|----------------------------|---------------------|
| 1   | 0.9488 | 0.0286 | 30                  | 1.4422                     | 0.9735              |
|     |        |        | 40                  | 1.4342                     | 0.8621              |
|     |        |        | 50                  | 1.4290                     | 0.7812              |
|     |        |        | 60                  | 1.4219                     | 0.7111              |
| 2   | 0.0396 | 0.9340 | 30                  | 0.83923                    | 3.618               |
|     |        |        | 40                  | 0.83435                    | 2.760               |
|     |        |        | 50                  | 0.83234                    | 2.166               |
|     |        |        | 60                  | 0.83165                    | 1.734               |
| 3   | 0.0487 | 0.0411 | 30                  | 0.85210                    | 5.490               |
|     |        |        | 40                  | 0.84077                    | 4.000               |
|     |        |        | 50                  | 0.83889                    | 3.071               |
|     |        |        | 60                  | 0.83860                    | 2.412               |
| 4   | 0.0839 | 0.6363 | 30                  | 0.86371                    | 3.793               |
|     |        |        | 40                  | 0.85907                    | 2.909               |
|     |        |        | 50                  | 0.85536                    | 2.258               |
|     |        |        | 60                  | 0.85274                    | 1.815               |
| 5   | 0.4220 | 0.0711 | 30                  | 1.0444                     | 2.498               |
|     |        |        | 40                  | 1.0385                     | 2.001               |
|     |        |        | 50                  | 1.0333                     | 1.646               |
|     |        |        | 60                  | 1.0287                     | 1.376               |
| 6   | 0.6483 | 0.3036 | 30                  | 1.2200                     | 1.371               |
|     |        |        | 40                  | 1.2136                     | 1.178               |
|     |        |        | 50                  | 1.2099                     | 1.019               |
|     |        |        | 60                  | 1.2072                     | 0.9144              |
| 7   | 0.3984 | 0.3358 | 30                  | 1.0423                     | 2.156               |
|     |        |        | 40                  | 1.0331                     | 1.735               |
|     |        |        | 50                  | 1.0249                     | 1.463               |
|     |        |        | 60                  | 1.0166                     | 1.217               |
| 8   | 0.1680 | 0.4957 | 30                  | 0.90832                    | 3.473               |
|     |        |        | 40                  | 0.90175                    | 2.672               |
|     |        |        | 50                  | 0.89853                    | 2.119               |
|     |        |        | 60                  | 0.89794                    | 1.733               |
| 9   | 0.2417 | 0.5433 | 30                  | 0.95304                    | 2.897               |
|     |        |        | 40                  | 0.94710                    | 2.295               |
|     |        |        | 50                  | 0.94451                    | 1.814               |
|     |        |        | 60                  | 0.94285                    | 1.486               |
| 10  | 0.3371 | 0.2131 | 30                  | 1.0010                     | 2.824               |
|     |        |        | 40                  | 0.99470                    | 2.248               |
|     |        |        | 50                  | 0.99081                    | 1.808               |
|     |        |        | 60                  | 0.98894                    | 1.472               |
| 11  | 0.4856 | 0.1364 | 30                  | 1.0889                     | 2.071               |
|     |        |        | 40                  | 1.0838                     | 1.719               |
|     |        |        | 50                  | 1.0800                     | 1.432               |
|     |        |        | 60                  | 1.0776                     | 1.219               |
| 12  | 0.5227 | 0.3776 | 30                  | 1.1319                     | 1.700               |
|     |        |        | 40                  | 1.1252                     | 1.401               |
|     |        |        | 50                  | 1.1204                     | 1.200               |
|     |        |        | 60                  | 1.1165                     | 1.030               |
| 13  | 0.5982 | 0.2521 | 30                  | 1.1697                     | 1.553               |
|     |        |        | 40                  | 1.1663                     | 1.315               |
|     |        |        | 50                  | 1.1639                     | 1.126               |
|     |        |        | 60                  | 1.1619                     | 0.9719              |

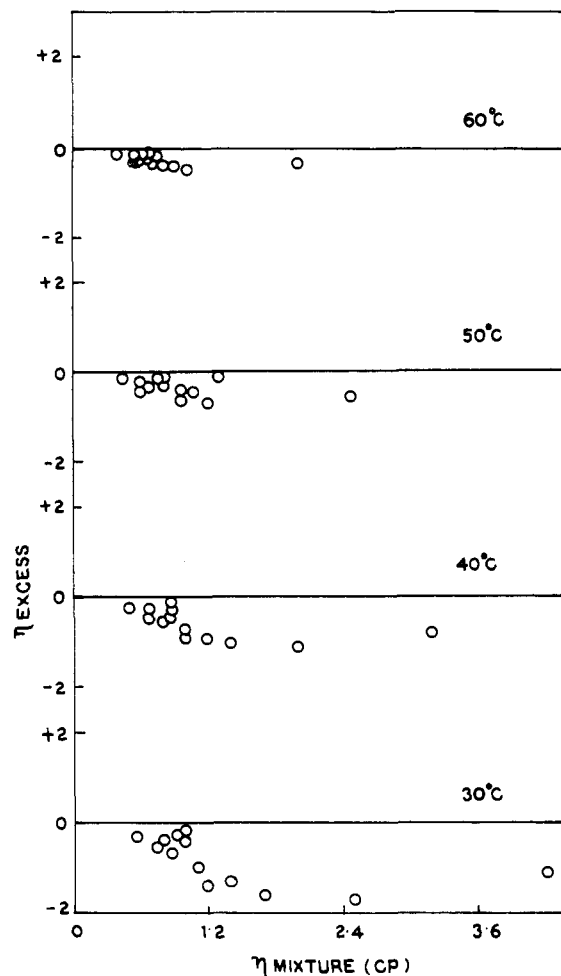
The highest temperature level was restricted to 60 °C in order to avoid errors due to evaporation losses during the experimental work.

The molecules of one or more of the components forming the ternaries are either polar or associating and accordingly show nonideal behaviors in mixtures. The nonidealities as reflected in mixture viscosities are expressed in terms of excess viscosity  $\eta^E$  given by the following equation

$$\eta^E = \eta_m - \sum X_i \eta_i \quad (1)$$

where  $\eta$  is the viscosity,  $X$  is the component mole fraction while superscript E stands for excess and subscript  $i$  and  $m$  stand for pure component and the mixture, respectively. With  $\eta-X_i-T$  data from Tables I-IV and eq 1, the corresponding  $\eta^E-X_i-T$  data were calculated.

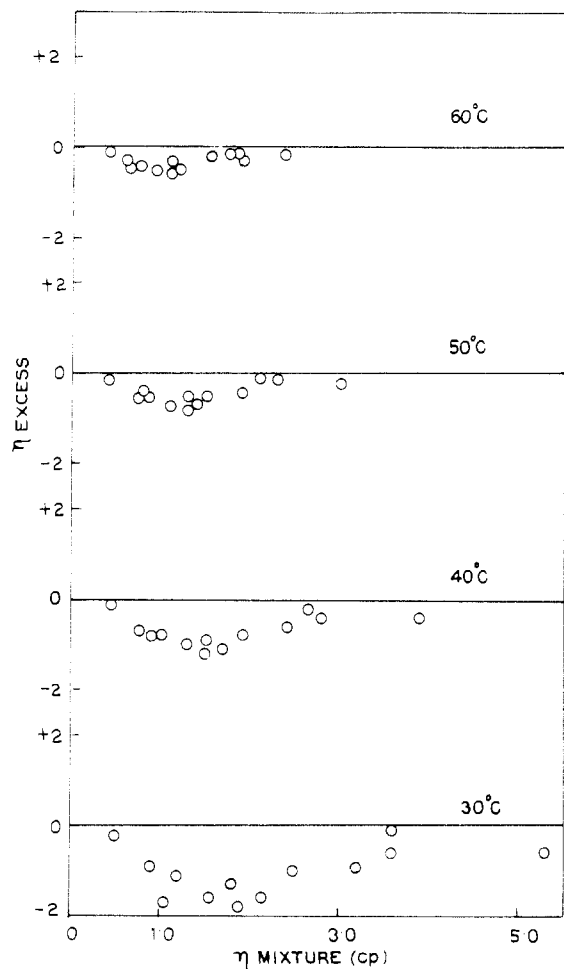
Figures 1-3 show the plots of  $\eta^E$  vs  $\eta_m$ . Negative values of  $\eta^E$  in most of the cases are the consequence of lower viscosity

**Figure 1.** Plot of excess viscosity against corresponding mixture viscosity for the ternary toluene (1)-bromobenzene (2)-1-octanol (3) at 30, 40, 50, and 60 °C.**Table IV. Experimental Densities and Viscosities for Pure Components of the Ternaries**

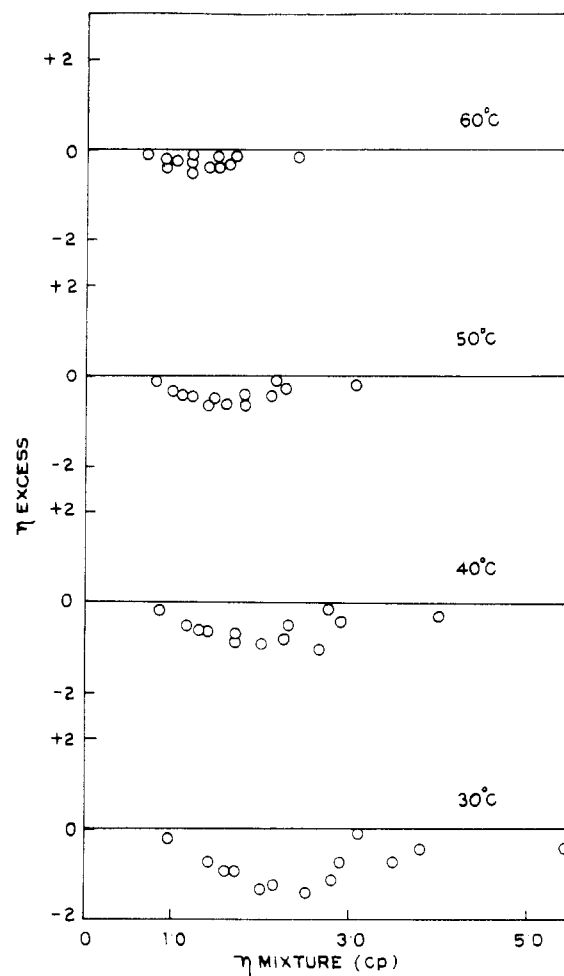
| pure component | $t, ^\circ\text{C}$ | $\rho, \text{g mL}^{-1}$ | $\eta, \text{cP}$     | ref |
|----------------|---------------------|--------------------------|-----------------------|-----|
| toluene        | 25                  | 0.8623                   | 0.5520                | 12  |
|                |                     | (0.86231)                | (0.5516)              |     |
|                |                     | 0.86696                  | 0.5372                |     |
|                |                     | 0.85473                  | 0.4851                |     |
|                |                     | 0.84969                  | 0.4272                |     |
|                |                     | 0.84750                  | 0.3905                |     |
| bromobenzene   | 25                  | 1.4965                   | 1.045                 | 12  |
|                |                     | (1.48820)                | (1.0430)              |     |
|                |                     | 1.4889                   | 0.9850                |     |
|                |                     | 1.4748                   | 0.8744                |     |
|                |                     | 1.4610                   | 0.7819                |     |
|                |                     | 1.4470                   | 0.7129                |     |
| 1-hexanol      | 25                  | 0.8160                   | 4.590                 | 12  |
|                |                     | (0.81590)                | (4.5920)              |     |
|                |                     | 0.81353                  | 3.765                 |     |
|                |                     | 0.81050                  | 2.934                 |     |
|                |                     | 0.80650                  | 2.169                 |     |
|                |                     | 0.80340                  | 1.655                 |     |
| 1-octanol      | 25                  | 0.8262                   | 6.298 <sup>a</sup>    | 12  |
|                |                     | (0.82209)                | (6.125 <sup>a</sup> ) |     |
|                |                     | 0.82392                  | 6.298                 |     |
|                |                     | 0.81926                  | 4.577                 |     |
|                |                     | 0.81472                  | 3.428                 |     |
|                |                     | 0.81039                  | 2.678                 |     |

<sup>a</sup> At 30 °C.

contributions of similar nonspecific interactions and H-bonding effects of molecular species in real mixtures rather than those in the corresponding ideal mixtures.



**Figure 2.** Plot of excess viscosity against corresponding mixture viscosity for the ternary toluene (1)-1-hexanol (2)-1-octanol (3) at 30, 40, 50, and 60 °C.



**Figure 3.** Plot of excess viscosity against corresponding mixture viscosity for the ternary bromobenzene (1)-1-hexanol (2)-1-octanol (3) at 30, 40, 50, and 60 °C.

**Table V.** Values of Binary Polynomial Constants  $A_{ij}$ ,  $B_{ij}$ ,  $C_{ij}$  and Additional Ternary Constant  $A^*_{ijk}$  Used in Equation 2 at Different Temperatures<sup>a</sup>

| systems                                      | parameter   | 30 °C   | 40 °C   | 50 °C   | 60 °C   |
|--|-------------|---------|---------|---------|---------|
| toluene (1)-bromobenzene (2) <sup>b</sup>    | $A_{12}$    | -0.2687 | -0.2215 | -0.1252 | -0.1535 |
|  | $B_{12}$    | -0.4618 | -0.4316 | -0.3819 | -0.1741 |
|  | $C_{12}$    | 0.6807  | 0.6537  | 0.5806  | -0.5685 |
| bromobenzene (1)-1-octanol (2)               | $A_{12}$    | -7.0851 | -4.7740 | -3.3477 | -2.6436 |
|  | $B_{12}$    | 1.2492  | 0.3444  | -0.3452 | -0.6920 |
|  | $C_{12}$    | -3.7390 | -3.5998 | -2.8254 | -2.4515 |
| toluene (1)-1-octanol (2)                    | $A_{12}$    | -7.3819 | -4.8729 | -3.3106 | -2.5434 |
|  | $B_{12}$    | 3.3259  | 2.1651  | 1.3623  | 0.9412  |
|  | $C_{12}$    | 0.9632  | -0.9081 | -0.5458 | -0.6506 |
| toluene (1)-1-hexanol (2)                    | $A_{12}$    | -3.8947 | -2.9628 | -2.0096 | -1.5114 |
|  | $B_{12}$    | 1.3869  | 1.2676  | 0.7865  | 0.2333  |
|  | $C_{12}$    | -3.8947 | -0.6250 | -0.5634 | -0.0897 |
| 1-hexanol (1)-1-octanol (2)                  | $A_{12}$    | -0.0023 | -0.0855 | -0.0801 | 0.0999  |
|  | $B_{12}$    | 2.2728  | 1.2523  | 1.5697  | 1.5038  |
|  | $C_{12}$    | 1.1830  | 1.1972  | 1.3014  | 0.8312  |
| bromobenzene (1)-1-hexanol (2)               | $A_{12}$    | -3.0760 | -2.2790 | -1.3397 | -0.7798 |
|  | $B_{12}$    | 0.8089  | 0.8572  | 0.1168  | -0.1247 |
|  | $C_{12}$    | -0.0898 | -0.6156 | 0.1474  | 0.1338  |
| toluene (1)-bromobenzene (2)-1-octanol (3)   | $A^*_{123}$ | 11.652  | 9.620   | 7.836   | 8.425   |
| toluene (1)-1-hexanol (2)-1-octanol (3)      | $A^*_{123}$ | -3.522  | -3.564  | -0.451  | 1.273   |
| bromobenzene (1)-1-hexanol (2)-1-octanol (3) | $A^*_{123}$ | 1.964   | 2.894   | 3.394   | 3.329   |

<sup>a</sup> Reference 11. <sup>b</sup> If binary toluene (1)-bromobenzene (2) is changed to bromobenzene (1)-toluene (2), then the values of  $A_{ij}$  and  $C_{ij}$  will remain the same. The value of  $B_{ij}$  will remain the same but its sign will change.

The ternary  $\eta$ - $X$ - $T$  data were fitted in eq 2, which includes the contributions of each constituent binary as calculated by a three-parameter Redlich-Kister-type equation (10, 11) along with a ternary contribution term besides the contribution on an ideal mixture basis. The  $A_{ij}$ ,  $B_{ij}$ , and  $C_{ij}$  were determined by

$$\eta_m = \sum_i X_i \eta_i + \sum_{i \neq j} X_i X_j [A_{ij} + B_{ij}(X_j - X_i) + C_{ij}(X_j - X_i)^2] + X_i X_j X_k A^*_{ijk} \quad (2)$$

least-squares method for the constituent binary using corre-

**Table VI. Root Mean Square (rms) Deviations for Different Ternary Systems with Use of Equation 2 at Different Temperatures**

|  | rms <sup>a</sup> |        |        |        | mean   |
|--|------------------|--------|--------|--------|--------|
|  | 30 °C            | 40 °C  | 50 °C  | 60 °C  |        |
| toluene (1)-bromobenzene (2)-1-octanol (3)   | 0.0845           | 0.0787 | 0.0796 | 0.0911 | 0.0835 |
| toluene (1)-1-hexanol (2)-1-octanol (3)      | 0.0606           | 0.0423 | 0.0351 | 0.0449 | 0.0457 |
| bromobenzene (1)-1-hexanol (2)-1-octanol (3) | 0.0465           | 0.0434 | 0.0499 | 0.0547 | 0.0485 |

<sup>a</sup> rms deviation =  $[\sum d_i^2/n]^{1/2}$  where  $n$  is the number of observations and  $d = [(\eta_{\text{exptl}} - \eta_{\text{calcd}})/\eta_{\text{exptl}}]$ .

sponding binary  $\eta_m-X-T$  data (11).  $A^*_{ijk}$  of eq 2 is the additional ternary constant to be evaluated by experimental ternary  $\eta_m-X-T$  data by the least-squares method. Such values of  $A_{ij}$ ,  $B_{ij}$ ,  $C_{ij}$ , and  $A^*_{ijk}$  are listed in Table V. The parameters included in Table IV were used as input in eq 2 for calculating  $\eta-X-T$  data showing root mean square deviations as listed in Table VI.

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#### Glossary

|     |                 |
|-----|-----------------|
| $T$ | temperature, K  |
| $t$ | temperature, °C |
| $X$ | mole fraction   |

#### Greek Letters

|        |                             |
|--------|-----------------------------|
| $\eta$ | absolute viscosity, cP      |
| $\rho$ | density, g mL <sup>-1</sup> |

#### Subscripts

|     |                        |
|-----|------------------------|
| $i$ | component in a mixture |
|-----|------------------------|

|       |                               |
|-------|-------------------------------|
| $m$   | mixture                       |
| 1,2,3 | component number in a mixture |

#### Superscript

|   |                 |
|---|-----------------|
| E | excess quantity |
|---|-----------------|

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## NEW COMPOUNDS

### Synthesis of 1-Aryl-2-hydrazino-4-phenyl-1,6-dihydro-1,3,5-triazine-6-thiones and Related Thiosemicarbazides

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#### Different

**1-aryl-2-(benzylthio)-4-phenyl-1,6-dihydro-1,3,5-triazine-6-thiones have been synthesized by known methods. These triazines on treatment with hydrazine hydrate under suitable conditions afforded corresponding hydrazino derivatives.**

**1-Aryl-2-hydrazino-4-phenyl-1,6-dihydro-1,3,5-triazine-6-thione on interaction with aryl/alkyl isothiocyanates gave related thiosemicarbazides.**

The presence of antituberculous (1, 2), antibacterial, antiviral (3), and antifungal (4) activity in some substituted thiosemicarbazides prompted us to search for new members of this series containing the triazinyl moiety.

The present paper deals with the synthesis of 1-aryl-2-hydrazino-4-phenyl-1,6-dihydro-1,3,5-triazine-6-thiones (II) and *N*-aryl/alkyl-*N'*-(1-aryl-4-phenyl-1,6-dihydro-6-thioxo-1,3,5-triazin-2-yl)thiosemicarbazides (III). The precursor 1-aryl-2-(benzylthio)-4-phenyl-1,6-dihydro-1,3,5-triazine-6-thione (I) was obtained by condensation of benzoyl isothiocyanate (5) and